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Production and purification of a calcium-dependent protease from *Bacillus cereus* BG1

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Abstract The production and purification of a calciumdependent protease by Bacillus cereus BG1 were studied. The production of the protease was found to depend specifically on the calcium concentration in the culture medium. This suggests that this metal ion is essential for the induction of protease production and/or stabilisation of the enzyme after synthesis. The calcium requirement is highly specific since other metal ions (such as Mg^{2+} and Ba^{2+} , which both activate the enzyme) are not able to induce protease production. The most appropriate medium for growth and protease production comprises (g L^{-1}) starch 5, CaCl₂ 2, yeast extract 2, K₂HPO₄ 0.2 and KH₂PO₄ 0.2. The protease of BG1 strain was purified to homogeneity by ultrafiltration, heat treatment, gel filtration on Sephacryl S-200, ion exchange chromatography on DEAE-cellulose and, finally, a second gel filtration on Sephacryl S-200, with a 39-fold increase in specific activity and 23% recovery. The molecular weight was estimated to be 34 kDa on SDS-PAGE. The optimum temperature and pH of the purified enzyme were determined to be 60°C and 8.0. respectively, in 100 mM Tris-HCl buffer + 2 mM CaCl₂.

Keywords Protease · *Bacillus cereus* · Calcium-dependent protease · Purification

Introduction

Proteases constitute one of the most important groups of industrial enzymes. They have diverse applications in a wide variety of industries such as the detergent, food, agrochemical and pharmaceutical industries [12, 15, 26].

Bacteria, moulds and yeasts are some of the microorganisms that produce proteases. Among bacteria, *Bacillus* strains are the most important producers of commercial proteases [11, 22].

Protease production depends on many factors. For instance, the growth rate of the culture and the composition of the medium play important roles. Indeed, carbon and nitrogen sources were considered determinant factors [6, 10]. Several studies have reported that proteins and peptides are necessary for effective protease production, while glucose repressed protease formation [4, 5, 7]. However, some works reported better protease synthesis in the presence of glucose as carbon source [8, 20]. Gessesse and Gashe [8] showed that the alkaliphilic strain of microbacterium isolated from an alkaline soda lake is insensitive to repression by glucose. Other medium compounds, such as metal ions and phosphorus source may also affect the amount of enzyme formation. Secades et al. [23] reported the production of a calciuminduced metalloprotease from the fish pathogen Flavo*bacterium psychrophilum*. The enzyme was detected only when the strain was cultivated in the presence of calcium.

Several alkaline proteases from the genus *Bacillus* have been purified and characterised [5, 24]. However, few reports are available on proteolytic enzymes from *Bacillus cereus*. Hayano et al. [13] reported a neutral metalloprotease from *B. cereus*. The DNA sequence of the *B. cereus* thermolysin-like enzyme has a high degree of homology with the sequences of other metalloproteases, especially with the gene for neutral protease from *Bacillus thuringiensis* (97% homology over 945 bp [3]).

In a previous search for alkaline-protease-producing strains, which have potential industrial applications, *B. cereus* BG1 strain, producing an organic solvent-stable protease, was isolated from an activated sludge reactor treating fishing industry wastewater [9]. The protease activity and thermal stability were dependent on calcium ions. At 60° C, Ca^{2+} (2 mM) stimulated the protease

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activity by 500%. In the presence of 10 mM Ca^{2+} , the enzyme retained 100, 93 and 26% of its initial activity after being heated for 15 min at 55, 60 and 70°C, respectively. However, the enzyme was completely inactivated when incubated at 55°C for 15 min in the absence of calcium.

In this paper, we describe the production and purification of a calcium-dependant protease from *B. cereus* BG1.

Materials and methods

Bacterial strain

The strain used in this study was isolated from an activated sludge reactor treating fishing industry wastewater. It was identified as *B. cereus* BG1.

Cultivation and media

The medium used for isolation of protease-producing strains was composed of $(g L^{-1})$: peptone, 5; yeast extract, 3; skimmed milk, 250 ml and bacteriological agar, 12. Inocula were routinely grown in Luria-Bertani (LB) broth medium $(g L^{-1})$: peptone, 10; yeast extract, 5 and NaCl, 5 [21]. The initial medium for protease production (M1) was composed of $(g L^{-1})$: carbon source, 10; CaCl₂, 1; yeast extract, 2; K₂HPO₄, 0.1; and KH₂PO₄ 0.1, pH 8.0. Media were autoclaved at 120°C for 20 min.

Cultivations were performed on a rotatory shaker (200 rev min⁻¹) for 48 h at 37°C, in 250 mL conical flasks with a working volume of 25 mL. The cultures were centrifuged and the supernatants were used for estimation of proteolytic activity.

Cell growth determination

The growth of the microorganism was determined by measuring optical density at 600 nm. All experiments were carried out in duplicate and repeated at least twice.

Protease purification

The culture broth was centrifuged and the cell-free supernatant (41 mL at 4,000 U mL⁻¹) was concentrated to 2 ml by ultrafiltration using a 10-kDa membrane.

The concentrated enzyme was then heat-treated in a water bath at 60°C for 30 min in the presence of 10 mM CaCl₂. Insoluble material was separated by centrifugation at 13,000 g for 10 min. The supernatant was then subjected to gel filtration on a Sephacryl S-200 column (3×100 cm) pre-equilibrated with 25 mM Tris-HCl (pH 8.0), 2 mM CaCl₂ and 0.025% Triton X-100 (buffer A). Fractions of 4 ml each were collected at a rate flow

of 30 mL h^{-1} and analysed for protease activity and protein concentration.

Fractions showing protease activities were pooled (56 mL) from the Sephacryl S-200 column and applied to a DEAE-cellulose column (3×25 cm) pre-equilibrated with 25 mM Tris-HCl (pH 8.5), 2 mM CaCl₂ (buffer B). The unadsorbed protein fractions were eluted with buffer B (150 mL). The chromatography was carried out at a flow rate of 45 mL h⁻¹. Fractions containing protease activity were pooled, concentrated by ultrafiltration to 2.3 mL as described previously and applied to a second Sephacryl S-200 column (2×160 cm) equilibrated with buffer A, and eluted at a flow rate of 0.46 mL min⁻¹. Fractions of 4.5 mL were collected.

All the purification steps were conducted at temperatures not exceeding 4°C.

Polyacrylamide gel electrophoresis

Sodium dodecyl sulphate-polyacrylamide gel electrophoresis (SDS-PAGE) was carried out for the determination of purity and molecular weight of the enzyme as described by Laemmli [17]. The molecular weight of the enzyme was calculated using a low molecular weight calibration kit (Lot 100K9314: Sigma, St Louis, Mo.) as markers. The molecular mass markers used were: bovine serum albumin (BSA; 66,000), egg white ovalbumin (45,000), glyceraldehyde-3-P dehydrogenase (36,000), bovine carbonic anhydrase (29,000), bovine trypsinogen (24,000), soybean trypsin inhibitor (20,100) and bovine α -lactalbumin (14,200). Protein bands were visualised after staining with Coomassie Brilliant blue R250.

Influence of pH and temperature on protease activity

The pH and temperature optima of the purified enzyme were determined with casein as substrate. The optimum pH for activity was studied in the range of 6-12 at 60° C. The effect of temperature on protease activity was studied from 50° C to 75° C at pH 8.0 in the presence of 2 mM CaCl₂.

Assay of proteolytic activity

Protease activity was measured by the method of Kembhavi et al. [16] using casein as substrate. A 0.5 mL aliquot of the culture supernatant, suitably diluted, was mixed with 0.5 mL 100 mM Tris-HCl (pH 8.0) + 2 mM Ca²⁺ containing 1% casein, and incubated for 15 min at 60°C. The reaction was stopped by addition of 0.5 mL 20% trichloroacetic acid. The mixture was allowed to stand at room temperature for 15 min and then centrifuged at 10,000×g for 15 min to remove the precipitate. The absorbance was measured at 280 nm. A standard curve was generated using solutions of 0–

50 mg L^{-1} tyrosine. One unit of protease activity was defined as the amount of enzyme required to liberate 1 μ g tyrosine per millilitre in 1 min under the experimental conditions used.

Protein concentration

Protein concentration was determined by the method of Bradford [1] with BSA as a standard.

Results and discussion

Effect of different carbon sources on protease synthesis

Protease production was first tested in medium M1 containing different carbon sources at a concentration of 10 g L⁻¹. *B. cereus* BG1 strain grew well in media containing maltose, glucose and starch, and the proteolytic activity varied with each carbon source. As shown in Table 1, the best carbon source for protease production was starch $(3,393 \text{ U mL}^{-1})$, followed by maltose $(3,062 \text{ U mL}^{-1})$. In a similar study, Johnvesly and Naik [14] showed that soluble starch was the best carbon source for protease production by *Bacillus* sp. JB-99.

Enzyme production was significantly low $(1,094 \text{ and } 1,283 \text{ U mL}^{-1})$ when *B. cereus* strain was grown on lactose and saccharose, respectively, and was the same as that of the control without carbon source.

In the present study, glucose was found to be a good carbon source for the growth of the BG1 strain but this substrate repressed the synthesis of the enzyme. Johnvesly and Naik [14] also reported that 1% glucose completely repressed the synthesis of alkaline protease by *Bacillus* sp. JB-99. However, other studies showed better protease synthesis in the presence of glucose as carbon source [20].

Since starch was the best carbon source, the effect of various concentrations of starch on protease production was studied. The optimum concentration of starch for protease production was of 5 g L^{-1} ; further additions of starch decreased the level of protease while biomass increased (Table 2).

Table 2 Effect of starch concentration on protease production by *B. cereus* BG1. Cultures were conducted for 48 h at 37° C in M1 medium containing different concentrations of starch. Values are means of three independent experiments. Standard deviations were $\pm 2.5\%$ (based on three replicates)

Starch (g L ⁻¹)	0	2	5	10	15	20
Protease activity (U mL ⁻¹) Biomass A_{600} Yield (U g ⁻¹ substrate)	1,003 1.4	2,349 3.1 673	3,730 4.8 545	3,345 4.9 234	3,200 5.1 136	2,931 5.1 96

Effect of various nitrogen sources on protease synthesis

In general, both organic and inorganic nitrogen were used efficiently by Bacillus sp. for protease production. In the present study, different organic (casein peptone, yeast extract, casein, soy peptone and urea) and inorganic (ammonium sulphate) nitrogen sources, at a concentration of 2 g L^{-1} , were tested in a medium containing starch at 5 g L^{-1} as carbon source. As shown in Table 3, the best nitrogen source for protease production by this strain was yeast extract $(3,720 \text{ U mL}^{-1})$ followed by casein peptone (3,542 U mL⁻¹). These results also showed that the strain could produce protease efficiently from casein as nitrogen source $(3,076 \text{ U mL}^{-1})$, indicating that the strain can obtain its nitrogen requirement directly from undigested proteins. Enzyme production was significantly lower with ammonium sulphate and urea as nitrogen sources. This result differs from the findings of Do Nascimento and Martins [2], who reported maximum enzyme activity by thermophilic Bacillus sp. SMIA-2 with ammonium nitrate as inorganic nitrogen source, and found that protease production was repressed by organic nitrogen sources.

Based on these observations, yeast extract was selected and its various concentrations were tested for the production of protease. As shown in Table 4, the enrichment of growth medium with yeast extract enhanced significantly both bacterial growth and the protease production. Maximum activity was achieved at a concentration of 2 g L^{-1} (3,755 U m L^{-1}).

Table 1 Effect of different carbon sources (10 g L⁻¹) on protease activity and biomass production by *Bacillus cereus* BG1. Cultivations were performed for 48 h at 37°C in media consisting of (g L⁻¹): carbon source 10, CaCl₂ 1, yeast extract 2, K₂HPO₄ 0.1 and KH₂PO₄ 0.1. Values are means of three independent experiments. Standard deviations were $\pm 2.5\%$ (based on three replicates)

Carbon source	Maltose	Glucose	Saccharose	Starch	Lactose	None
Activity $(U mL^{-1})$	3,062	814	1,283	3,393	1,094	1,098
Biomass A_{600}	4.6	4.75	2.1	5.2	1.6	1.7

Table 3 Effect of different nitrogen sources (2 g L⁻¹) on protease and biomass production by *B. cereus* BG1. Cultivations were performed for 48 h at 37°C in media consisting of (g L⁻¹): starch 5, CaCl₂ 1, nitrogen source 2, K₂HPO₄ 0.1 and KH₂PO₄ 0.1. Values are means of three independent experiments. Standard deviations were $\pm 2.5\%$ (based on three replicates)

Nitrogen source	Ammonium sulphate	Yeast extract	Casein peptone	Soya peptone	Casein	Urea
Activity $(U m L^{-1})$	1,018	3,720	3,542	3,425	3,076	1,978
$\begin{array}{c} \text{(O IIIL)}\\ \text{Biomass}\\ A_{600} \end{array}$	1.9	5.13	2.9	5.06	3	2.5

Table 4 Effect of yeast extract concentration on protease production by *B. cereus* BG1. Cultivations were performed for 48 h at 37°C in media consisting of (g L⁻¹): starch 5, CaCl₂ 1, K₂HPO₄ 0.1, KH₂PO₄ 0.1 and different concentrations of yeast extract. Values are means of three independent experiments. Standard deviations $\pm 2.5\%$ (based on three replicates)

Yeast extract (g L ⁻¹)	0.5	1	2	3	5
Protease activity (U mL ⁻¹)	2072	2727	3755	3643	3690
Biomass A_{600}	2.24	2.93	4.82	5.12	4.86

Effect of metal ions on protease synthesis

Several studies have shown that divalent cations can stimulate or inhibit enzyme formation in microorganisms. Mabrouk et al. [19], reported that Ca^{2+} at 0.07% markedly affected protease production by *Bacillus licheniformis* ATCC 21415 and caused 26.6% increase in activity over the control.

The effects of addition of some inorganic salts to the culture at a concentration of 10 mM on growth and protease production by B. cereus BG1 are shown in Table 5. When the strain was grown in the absence of metal ions, no protease activity was detected in the culture supernatant, although such a medium yielded a higher concentration of biomass. Among all the inorganic salts tested, only CaCl₂ led to a strong increase in protease synthesis. The addition of CaCl₂ (10 mM) enhanced protease production to a level of $3,800 \text{ U mL}^{-1}$. Very low levels of activity-about 28 U mL⁻¹-were detected in medium containing MgSO₄, although the strain grew well in the presence of this divalent cation. However, with ZnSO₄, MnSO₄ and CuSO₄, growth was inhibited. Therefore, biosynthesis of protease by B. cereus BG1 can be considered calcium-dependent since other metals such as Ba^{2+} and Mg^{2+} , which stimulated protease activity, were unable to induce protease production.

In a second experiment, the strain was grown in the presence of different concentrations of CaCl₂ ranging from 0.05 g L to 10 g L⁻¹. As shown in Table 6, protease production was significantly lower with CaCl₂ concentrations up to 0.5 g L⁻¹. Maximum protease induction was observed with 2 g L⁻¹, about 4,036 U mL⁻¹, which was about 16-fold over the med-

Table 5 Effects of inorganic salts on the production of alkaline protease by *B. cereus* BG1. Cultivations were performed for 48 h at 37°C in media consisting of $(g L^{-1})$: starch 5, yeast extract 2, K₂HPO₄ 0.1, KH₂PO₄ 0.1 and metal ions 1. Values are means of three independent experiments. Standard deviations were $\pm 2.5\%$ (based on three replicates)

Metal ions (10 mM)	None	CaCl ₂	MgS04	CuS04	BaCl ₂	MnS04	ZnS04
Protease activity $(I \mid mI^{-1})$	0	3,800	28	0	58	0	0
Biomass A_{600}	1.9	4.72	2.97	0.5	0.89	0.54	0.43

Table 6 Effect of CaCl₂ concentration on protease and biomass production by *B. cereus* BG1. Cultivations were performed for 48 h at 37°C in media consisting of (g L⁻¹): starch 5, yeast extract 2, K₂HPO₄ 0.1, KH₂PO₄ 0.1 and different concentrations of CaCl₂. Values are means of three independent experiments. Standard deviations were $\pm 2.5\%$ (based on three replicates)

$CaCl_2$ (g L ⁻¹)	0	0.05	0.1	0.2	0.5	1	2	5	10
Activity $(U mL^{-1})$	0	116	160	254	3,389	3,760	4,036	3,447	2,385
Biomass A_{600}	2.3	4.7	4.8	4.74	4.6	4.6	4.6	4.7	4.9

ium containing 0.2 g L^{-1} CaCl₂. Beyond 2 g L^{-1} CaCl₂, protease activity decreased while biomass increased. These results clearly indicated that production of the BG1 protease is dependent on the CaCl₂ concentration.

Effect of the concentration of K_2HPO_4 and KH_2PO_4 on protease production

The amount of phosphorus source was also varied (Table 7). A high level of activity, about 3,710 U mL⁻¹, was detected in medium lacking a phosphorus source. Maximum protease was observed with 0.2 g L⁻¹ K₂HPO₄ and 0.2 g L⁻¹ KH₂PO₄. As the phosphorus level increased, the level of protease activity and bacterial growth decreased. Since Ca²⁺ has a significant stabilising effect on protease, the decrease in protease synthesis could be explained by the lowering of the available Ca²⁺ in the culture with increasing phosphorus phosphorus concentration.

Role of calcium in protease production

Minor studies have been conducted to investigate the biological role of calcium in enzyme production. Secades et al. [23] showed that the level of Fpp1 protease produced by *F. psychrophilum* is specifically dependent on the CaCl₂ concentration. We therefore examined three

Table 7 Effect of phosphorus source concentration on protease and biomass production by *B. cereus* BG1. Cultivations were performed for 48 h at 37°C in media consisting of (g L⁻¹): starch 5, yeast extract 2, CaCl₂ 2, and different concentrations of K₂HPO₄ and KH₂PO₄. Values are means of three independent experiments. Standard deviations were $\pm 2.5\%$ (based on three replicates)

					-		
KH_2PO_4	0	0.1	0.2	0.3	0.5	0.7	1
(g L) K_2HPO_4 $(g L^{-1})$	0	0.1	0.2	0.3	0.5	0.7	1
Activity $(U m I^{-1})$	3,709.1	3,941.8	4,218.2	4,072.7	2,858.2	581.8	102
$\begin{array}{c} \text{(O IIIL)}\\ \text{Biomass}\\ A_{600} \end{array}$	3.54	4.47	4.70	4.51	4.47	1.59	1.65

hypotheses that could explain the enhancement of protease synthesis by CaCl₂:

First hypothesis. Ca^{2+} might be required for enzyme secretion.

Second hypothesis. Enzyme production might be induced by calcium.

Third hypothesis. The active conformation of the enzyme might be stabilised by ionic calcium after synthesis.

The first hypothesis seems improbable since no activity was detected within the cells when the strain was grown in a medium lacking CaCl₂. Furthermore, no activity was detected in the culture supernatant and within the cells when they were grown in media containing MgCl₂. When cultivated in a medium containing CaCl₂, more than 88% of the enzyme activity was detected in the culture supernatant. In contrast to our results, Liao and McCallus [18] reported that more than 60% of the enzyme activity was retained within the cells when *Pseudomonas aeruginosa* CY091 was grown in a medium containing ZnCl₂, MgCl₂, or MnCl₂.

To study hypotheses concerning the induction or stabilisation of the enzyme by $CaCl_2$, additional experiments were conducted to elucidate the role of Ca^{2+} . In the first experiment the time-courses of protease production and growth of *B. cereus* BG1 were studied. As shown in Fig. 1, *B. cereus* BG1 grew well in medium supplemented with $CaCl_2$ and reached stationary phase after 15 h. Biosynthesis of protease by the strain appeared to be growth-related, since the activity was detected from early stages in the growth of the microorganism, with values increasing exponentially at



Time (h)	0	4	8	16	24
Protease activity	3,900	4,938	3,950	2,727	1,585
$(U mL^{-1})$ Biomass A_{600}	4.65	5.17	5.17	4.7	3.9

the end of the exponential phase, then continuing to increase even during stationary phase. These results differ from those of previous works, which showed that induction of metalloprotease from the fish pathogen F. *psychrophilum* was only growth related; addition of calcium during the stationary phase did not induce production of the enzyme [23].

Ca-induction experiments were also performed by incubating the microorganism in a medium composed of (g L^{-1}): starch 5, CaCl₂ 2, yeast extract 2, K₂HPO₄ 0.1 and KH₂PO₄ 0.1. During the exponential or stationary phases, $\bar{2}$ g L^{-1} CaCl₂ was added to the cultures after 4, 8, 16 and 24 h incubation. Protease production throughout this study was determined after 48 h of growth, which corresponds to the optimum period for enzyme production (Table 8). Furthermore, proteins in the culture supernatants were also analysed by SDS-PAGE (Fig. 2). As shown in Table 8 and Fig. 2, addition of CaCl₂ during the exponential and stationary phases resulted in the presence of the BG1 protease in the medium (the molecular weight of the purified protease was estimated to be approximately 34,000 by SDS-PAGE, see Fig. 6). Protease production was improved by 30% when CaCl₂ was applied during exponential



7 6 5 4 3 2 1 (kDa) (kD

Fig. 1 Time-course of alkaline protease production and growth of *Bacillus cereus* BG1 in 100 mL medium consisting of $(g L^{-1})$: starch 5, CaCl₂ 2, yeast extract 2, K₂HPO₄ 0.2 and KH₂PO₄ 0.2. Cell growth was measured by absorbance at 600 nm (A_{600}). Protease activity was determined in culture filtrates obtained after removal of cells by centrifugation, as described in Materials and methods. Values are means of three independent experiments. Standard deviations were less than 5%. *Arrows* Time-points of addition of 2 g L⁻¹ CaCl₂ in a subsequent experiment

Fig. 2 Electrophoretic analyses of supernatants from various cultures after acetone treatment. *B. cereus* was initially grown in medium consisting of (g L⁻¹): starch 5, CaCl₂ 2, yeast extract 2, K₂HPO₄ 0.1, KH₂PO₄ 0.1. Lanes: *I* Molecular weight markers, 2 culture conducted with 2 mM CaCl₂ initially; *3–6* cultures to which CaCl₂ was added after 4 h (*lane 3*), 8 h (*lane 4*), 16 h (*lane 5*) and 24 h (*lane 6*); 7 culture conducted in medium lacking CaCl₂





Fraction number

Fig. 3 Chromatography on Sephacryl S-200 of the concentrated and treated enzyme preparation. The enzyme preparation was applied to a 3×100 cm column, equilibrated and eluted with 25 mM Tris-HCl (pH 8.0), 2 mM CaCl₂ and 0.025% Triton X-100. Fractions (4 mL) collected from the column were assayed for protease activity. Flow rate = 0.5 mL min⁻¹



Fig. 4 Elution profile of *B. cereus* BG1 protease from a DEAEcellulose column. The column $(3\times25 \text{ cm})$ was equilibrated with 20 mM Tris-HCl (pH 8.0) and 2 mM CaCl₂. The unadsorbed protein fraction was eluted with the same buffer at a flow rate of 0.66 mL min⁻¹. The protease activity of each fraction was determined as described in Materials and methods

growth phase (4 h), compared to that obtained with the medium initially supplemented with $CaCl_2$. However, addition of $CaCl_2$ during stationary phase led to a significant reduction in enzyme formation.

No activity was detected when the strain was grown in medium lacking CaCl₂. However, a minor band, which migrated in SDS-PAGE to a position corresponding to a molecular weight of 34 kDa, was discernable. Furthermore, protein bands having molecular weight greater than 34 kDa, and other protein bands lower than 34 kDa, which may correspond to degradation products of the BG1 protease, were also observed. Therefore, the hypothesis that protease production is stimulated by calcium seems to be invalidated. From these results, and those showing that the thermoactivity and the thermostability of the



Fig. 5 Application of active fractions from DEAE-Cellulose to a second Sephacryl S-200 column. The enzyme preparation was applied to a 2×160 cm column, equilibrated and eluted with 25 mM Tris-HCl (pH 8.0), 2 mM CaCl₂ and 0.025% Triton X-100. Fractions (4 mL), collected from the column at a flow rate 0.46 mL min⁻¹, were assayed for protease activity



Fig. 6 SDS-PAGE of purified protease from *B. cereus* BG1. Lanes: *I* Molecular weight markers, *2* concentrated enzyme preparation, *3* purified BG1 protease (fraction 124)

enzyme were considerably increased in the presence of $CaCl_2$ [9], it seems likely that $CaCl_2$ is required for maintaining the molecular conformation needed for enzyme activity. On the other hand, enzyme activity inhibited by treatment with metal chelators such as EDTA, was not restored at all by the addition of calcium ions (2–50 mM). This suggests that the tertiary structure of the enzyme was irreversibly destroyed by chelating metal ion(s) in the protein molecule. These findings are in line with several earlier reports showing that the three-dimensional structure of the protease from *B. cereus* contains four Ca^{2+} binding sites [25].

Protease purification

In the first step, the culture supernatant obtained by centrifugation (13,000 g for 10 min at 4° C) was con-

Purification steps ^a	Total Protein (mg)	Total activity (U×10 ³)	Specific activity× 10^3 (U mg ⁻¹)	Recovery (%)	Purification (fold)
Cell-free culture supernatant	3.8	164	43.15	100	1
Ultrafiltration	2.7	141	52.22	86	1.21
Heat treatment	1.6	112	70	68	1.62
Sephacryl S-200	1.2	96	80	58.3	1.85
DEAE-cellulose chromatography	0.32	42	131.25	25.6	3.04
Second Sephacryl S-200	0.022	37	1,682	23	38.9

^aAll operations were carried out at 4°C



Fig. 7 Effect of pH on proteolytic activity. The pH profile was determined in different buffers by varying pH values at 60°C. Values are means of three independent experiments. Standard deviations were $\pm 2.5\%$ (based on three replicates)



Fig. 8 Effect of temperature on proteolytic activity. The temperature profile was determined by assaying protease activity at different temperature values (40–70°C). Values are means of three independent experiments. Standard deviations were $\pm 2.5\%$ (based on three replicates)

centrated by ultrafiltration using a 10-kDa membrane then heat treated. These two steps resulted in 1.6-fold purification, with a recovery of 68% and a specific activity of 70×10^3 U mg⁻¹. The heated enzyme was



Fig. 9 Effect of calcium on protease thermostability. Purified enzyme was preincubated at 60°C in the presence of various concentration of CaCl₂. Residual activity was determined from 0 to 60 min as described in Materials and methods. The non-heated enzyme was considered as control (100%). Values are means of three independent experiments. Standard deviations were $\pm 2.5\%$ (based on three replicates)

subjected to gel filtration on a Sephacryl S-200 column with buffer A. The elution profiles of protease and proteins from Sephacryl S-200 are shown in Fig. 3. This procedure yielded a single peak of protease activity.

Fractions containing protease activity were pooled, then loaded on a DEAE-cellulose column pre-equilibrated with buffer B. Protease activity appeared in a single peak together with unadsorbed fractions. The elution profile is shown in Fig. 4. Active fractions were pooled then concentrated by ultrafiltration before being applied to a second Sephacryl S-200 gel. The elution profile is shown in Fig. 5.

Active fractions eluted from the second Sephacryl S-200 gel filtration were assayed for activity, and fraction 124 was analysed on a 15% SDS-polyacrylamide gel. As shown in Fig. 6, a unique protein band was obtained. The molecular weight of the BG1 protease was estimated to be 34 kDa by SDS-PAGE using molecular weight markers.

The results of the purification procedure are summarised in Table 9. After the final purification step, the protease was purified 39-fold with a recovery of 23% and a specific activity of $1,682 \times 10^3$ U mg⁻¹.

Influence of pH and temperature on enzyme activity

The enzyme was active between pH 6.0 and 9.0, with an optimum at pH 8.0. At pH values 8.5 and 7.0, 75 and 32% activity remained, respectively (Fig. 7). The optimal temperature for the activity of the purified protease was 60°C, when incubated for 15 min at pH 8.0 (Fig. 8).

The thermostability of the purified protease was examined by incubating the enzyme at 60°C for 1 h in the presence of various concentrations of CaCl₂. As shown in Fig. 9, the stability of the enzyme was considerably enhanced by Ca²⁺. The half-life of the purified enzyme at 60°C was determined to be of the order of 23 and 51 min, in the presence of 1 and 2 mM CaCl₂, respectively.

Conclusion

This study described the production and purification of a calcium-dependent protease from *B. cereus* BG1. Protease activity was detected only when the cells were grown in medium containing $CaCl_2$. The biosynthesis of protease can be said to be absolutely calcium-dependent since no other divalent cation was able to induce enzyme production. The data presented here show that calcium might be required for stabilising the enzyme after synthesis. Further work is needed to confirm this hypothesis.

An optimised induction medium, which supported good growth as well as enzyme production, was formulated and consisted of (g L^{-1}): starch 5, CaCl₂ 2, yeast extract 2, K₂HPO₄ 0.2 and KH₂PO₄ 0.2.

The enzyme was purified to homogeneity by ultrafiltration, heat treatment, and gel filtration on Sephacryl S-200, DEAE-cellulose ion exchange chromatography, and by a second Sephacryl S-200 gel filtration chromatography. After the final purification step the enzyme was purified 39-fold with a specific activity of $1,682\times10^3$ U mg⁻¹ and 23 % recovery. The purified protease preparation was homogenous on SDS-PAGE and its molecular weight was estimated to be 34 kDa. The optimum pH and temperature for the proteolytic activity were pH 8.0 and 60°C, respectively.

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